

HYDROGEN GENERATION SYSTEM FOR DECENTRAL APPLICATIONS (HYGENESYS)

Ir. Hans Gelten

Projectmanager Lectoraat Duurzame Energievoorziening

Bas Hupjé

4th year student Chemical Engineering

Tjeerd Vogelzang

4th year student Applied Physics

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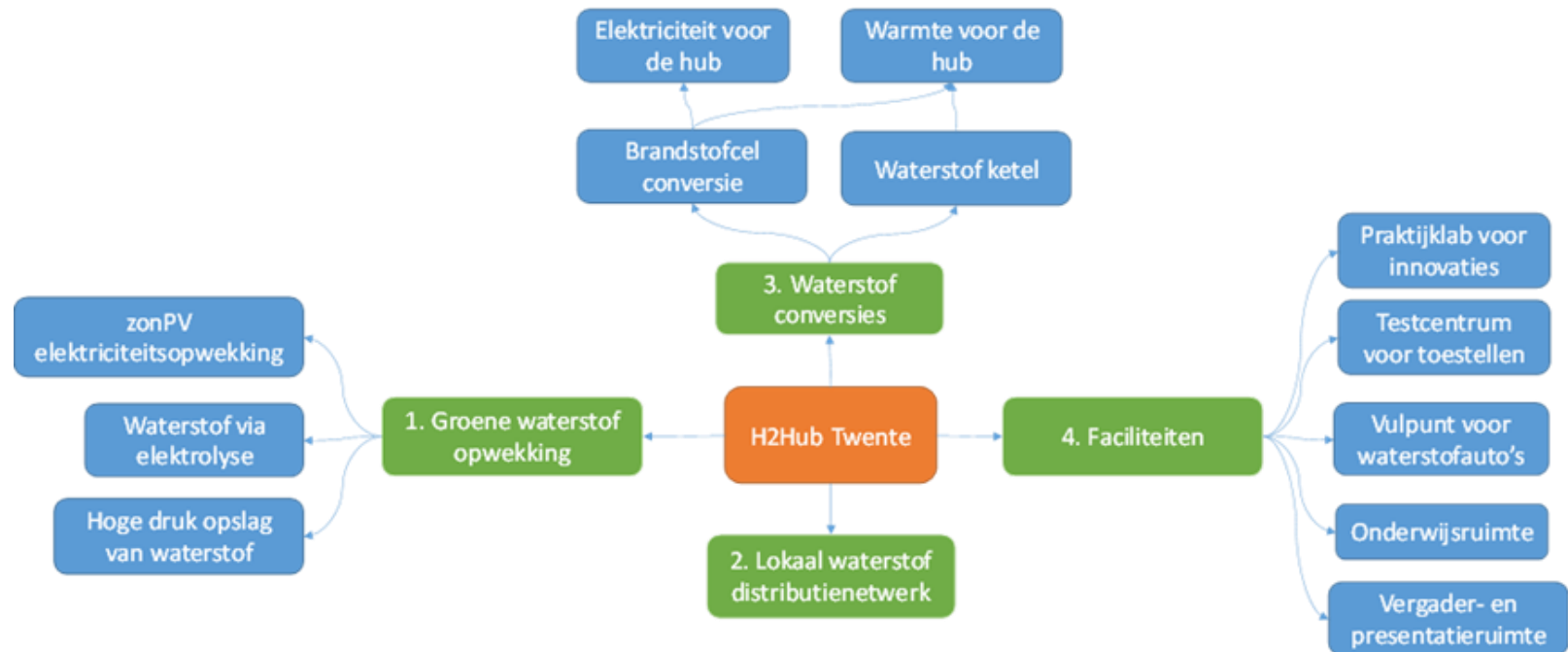
SPRONG

HAN + SAXION + company partners



- **Objective SPRONG application**
 - KIA development with partners in field labs (H2Hub, Grohw)
 - Strong Saxion/HAN research group, in 4 years to EU project
 - Building up 20 FTE together, 2 lectors
 - Larger projects (Think East Netherlands)
- **Key partners:**
 - Hogeschool Arnhem-Nijmegen (penvoerder)
 - Oost-NL
 - Cleantechregio waterstofroute
 - KIEMT
 - bedrijven GROHW initiatief Deventer
 - **bedrijven H₂Hub Twente**
 - VDL energy systems
 - Demcon
 - Universiteit Twente
 - ROC van Twente

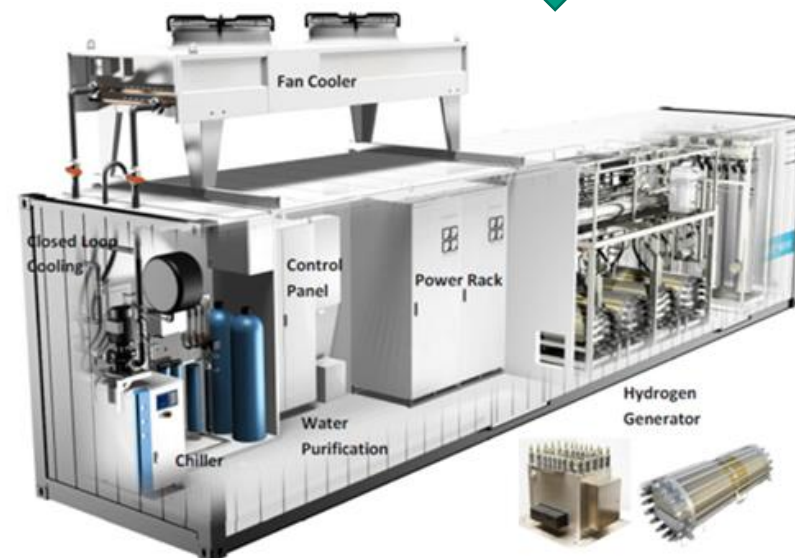
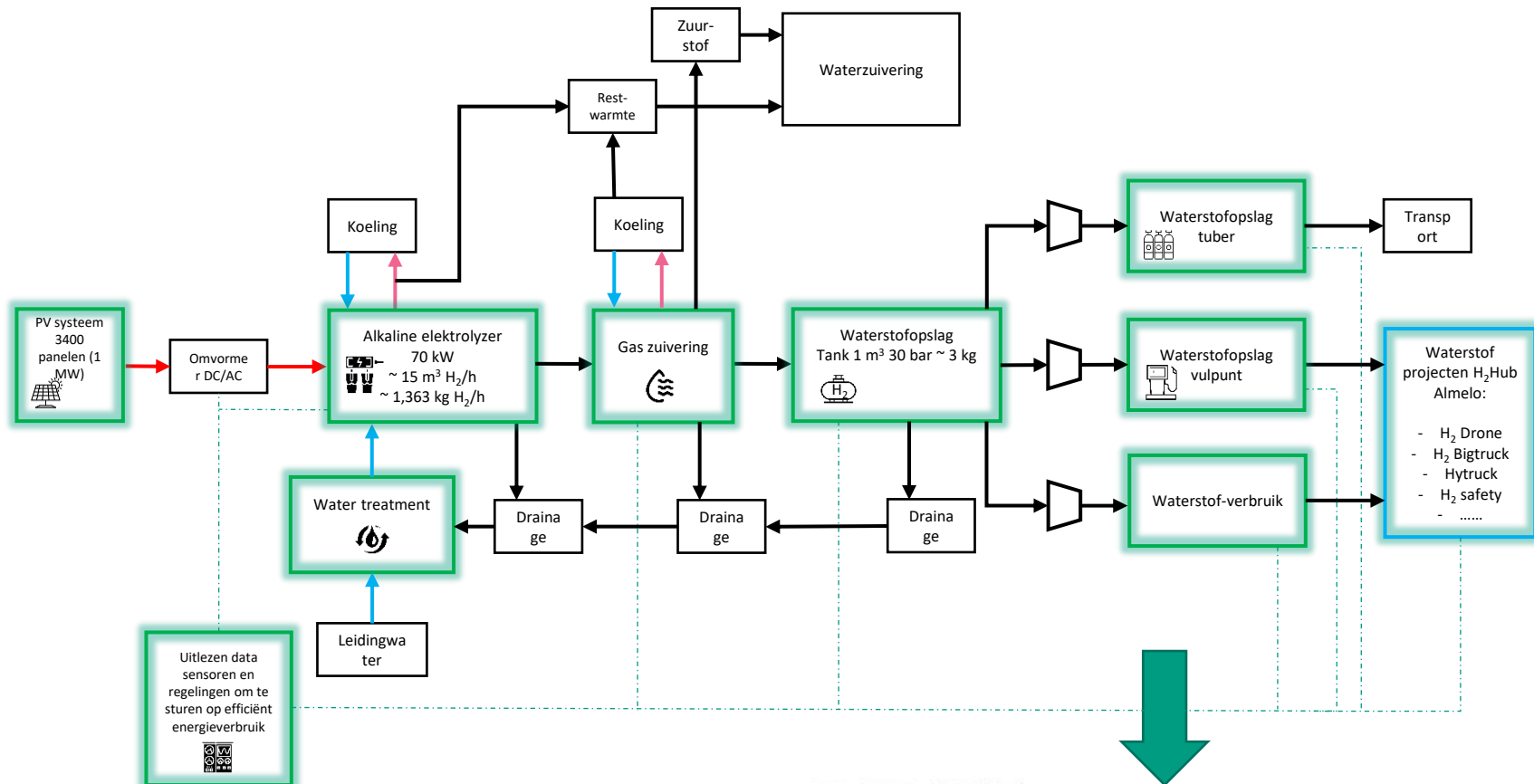
H₂Hub



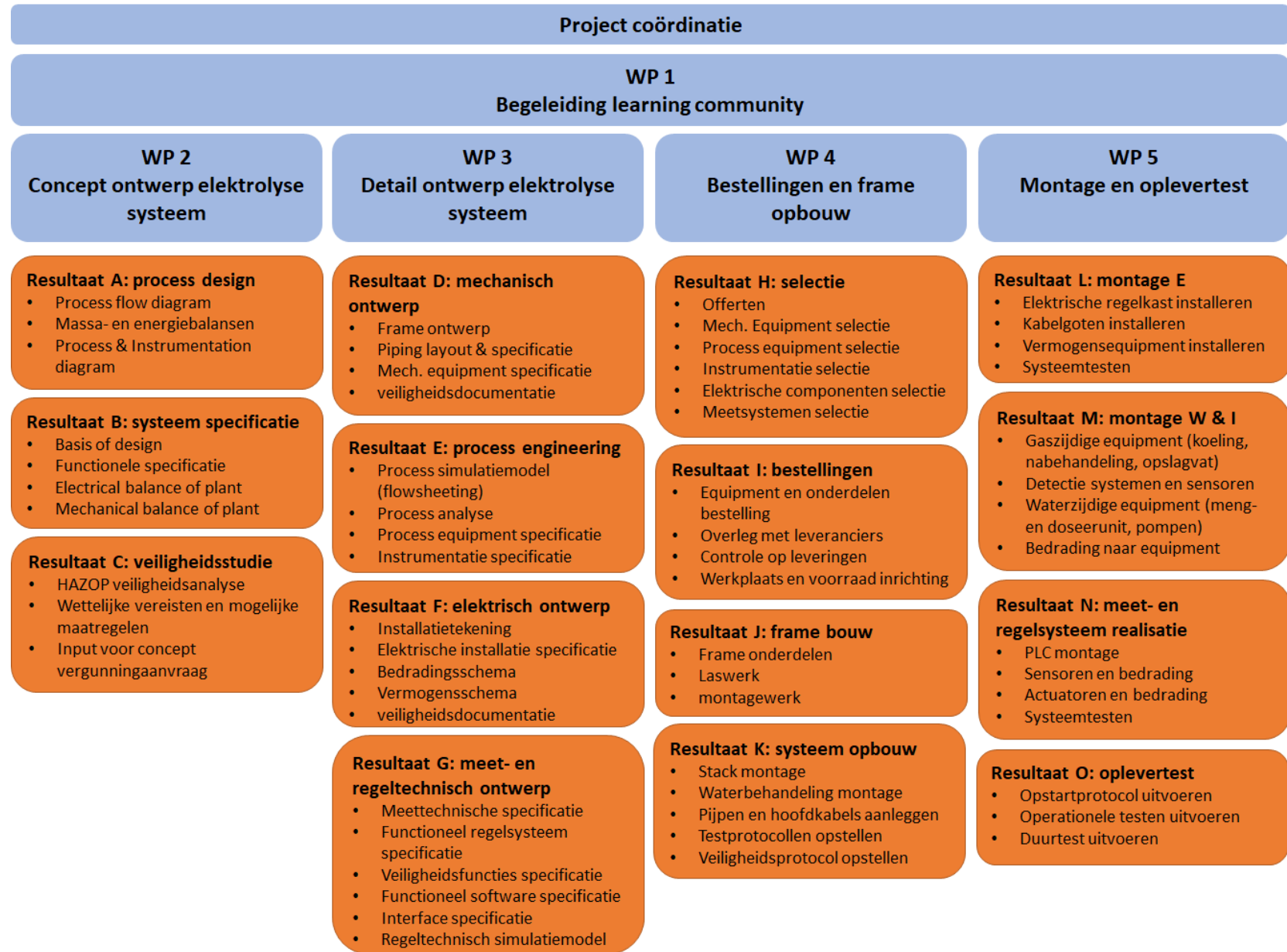
Project HYGENESYS



System overview H₂ electrolyzer



Overview WP's



Development and construction H₂ electrolyzer



- Lead time approx. 2 years, with successive project teams
- Students, lecturer-researchers & company employees (Learning Community)
- Different educational units can join:
 - Minor Engineering of Energy Systems
 - UT Master Sustainable Energy Technology (SET)
 - ROC installation technology & automotive
 - Smart solutions: business & communication
 - Internship and graduation projects from different levels
 -
- 'Logical' follow-up to the KIEM project HyWINN, in which exploratory research is being done into a decentralised Hydrogen supply and INNovatielab

Consortium

UNIVERSITY OF TWENTE.

roc van twente

SAXION HOGESCHOOL

HAN UNIVERSITY OF APPLIED SCIENCES



Nieuwe kennis en inzichten verwerken, delen en verrijken



Chemische Technologie
Werktuigbouwkunde
Technische natuurkunde
Elektrotechniek
Integrale veiligheidkunde

DEMCON powerspex
...het klopt al 23 jaar!

WATERSCHAP vechtstromen

kiemt

MACHINEFABRIEK Boessenkool
Osse Equipment Manufacturing Group

H₂ Hub Twente
Waterstof Platform

kiwa

VBL

coteq
NETBEHEER

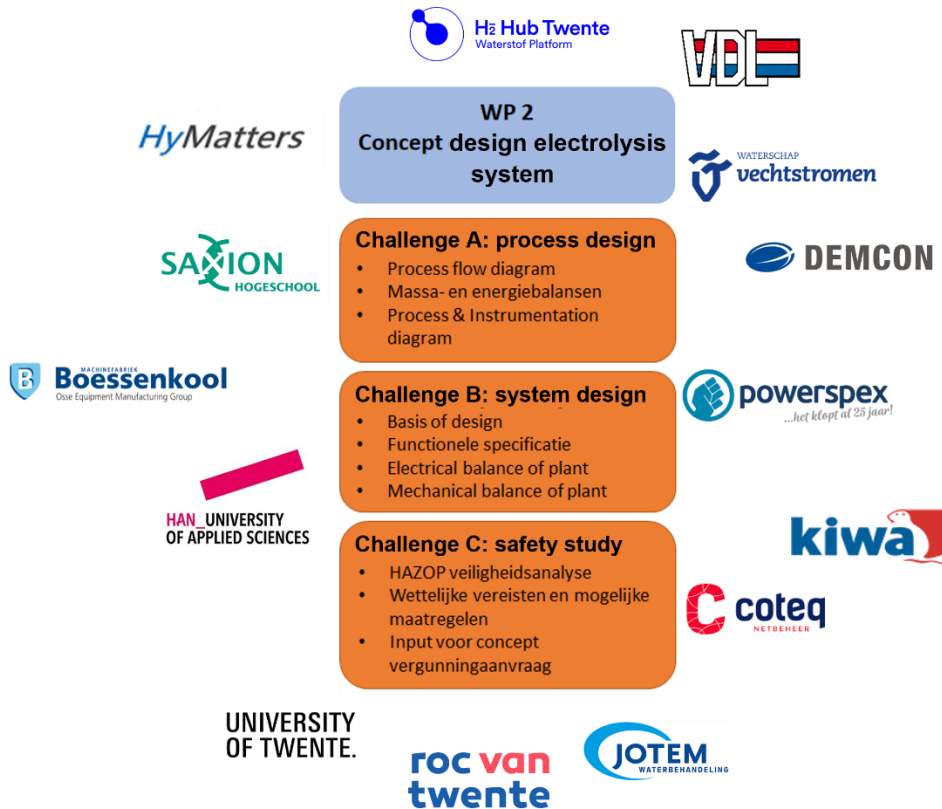
JOTEM
WATERBEHANDELING

HyMatters

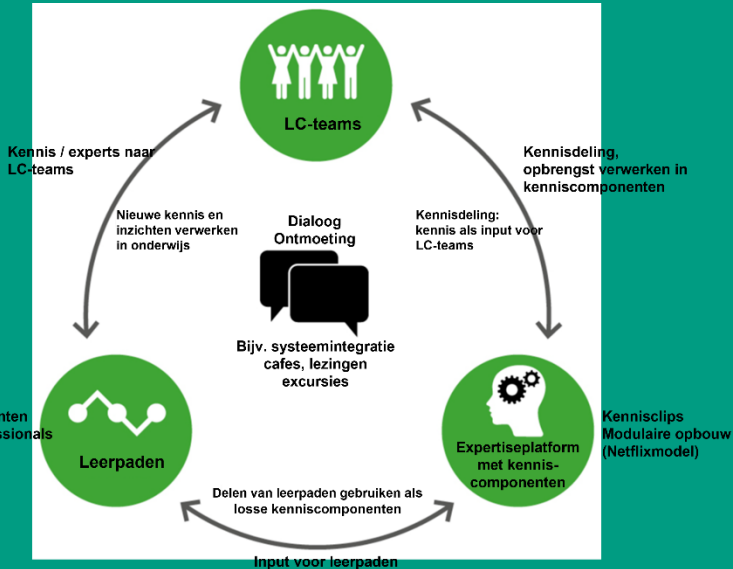
Learning Community



Developing a Learning Community



Learning Communities



- A challenged-based learning community for hydrogen development and application
- Building up knowledge and skills at:
 - Students (Saxion, UT, HAN , ROC)
 - Company employees
 - Lecturer/researchers
- Workshop for technical practical projects: “learning on the job”
- Developing a Knowledge Centre:
 - Knowledge meetings, Work sessions
 - Sharpening knowledge and innovation agenda with consortium/ecosystem
 - Development of successor projects
- Sustainability in large programmes such as SPRONG, VIE and Top Sector Energy (national)

Questions:
j.a.p.gelten@saxion.nl
06-10823289



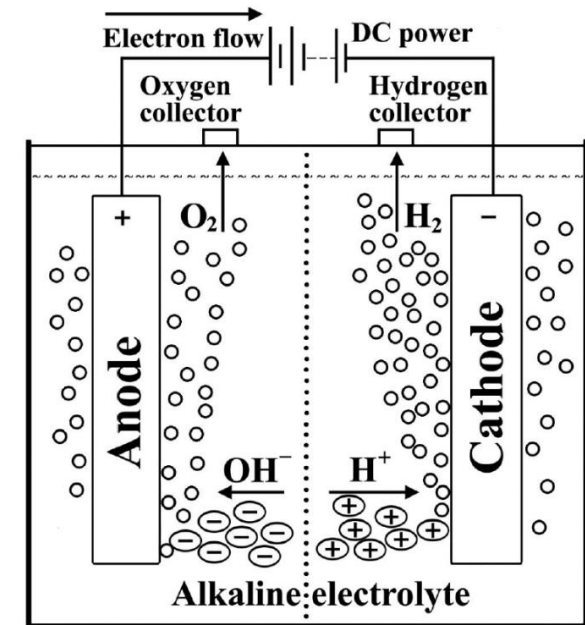
Project HYGENESYS – Design of Experiments

Tjeerd Vogelzang
4th year student Applied Physics



Introduction project

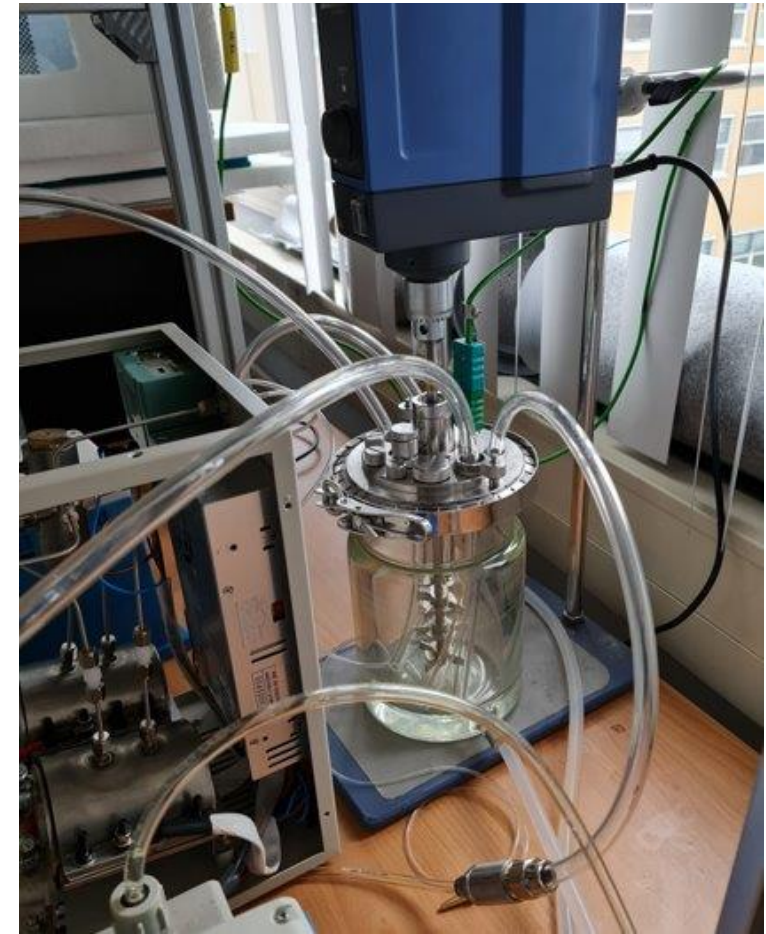
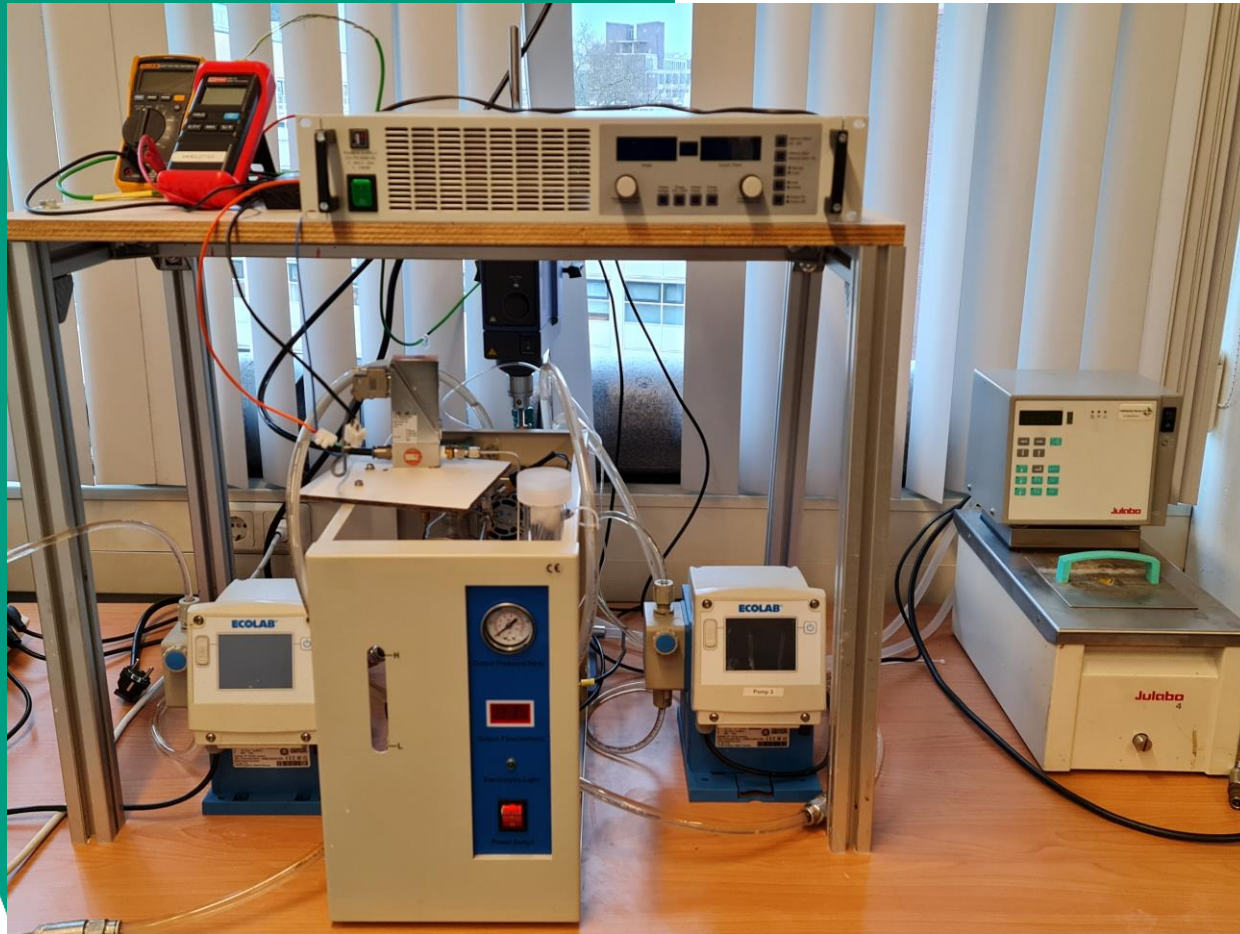
- Optimization alkaline electrolyzer
- Different parameters to determine the hydrogen production
- These parameters are:
 - Different lyes
 - Concentration
 - Temperature
 - Mass flow rate
 - Electric current



Approach

- Theory research
 - How does an electrolyser system work?
 - Which parameters have an effect on hydrogen production?
- Measuring method
 - MSA (measurement system analysis)
 - Reliable
 - Independent
- DOE / multifactorial design / residual analysis
 - Which parameters / repeats
 - Interactions
 - Useable results

Setup test system



Measurement system analysis (ml/min)

- Cp-gauge is 134.6
- The measurement system is excellent
 - The test system is sturdy

Measurements Gauge R&R containing 4 positions, 3 Operators and 3 Repeats			Parts / Positions											
			1: Setting 1			2: Setting 2			3: Setting 3			4: Setting 4		
			Repeat 1	Repeat 2	Repeat 3	Repeat 1	Repeat 2	Repeat 3	Repeat 1	Repeat 2	Repeat 3	Repeat 1	Repeat 2	Repeat 3
Operator	15	Day 1	180	180,9	180	531,1	531,1	531,1	532,1	532,1	532,1	313,87	314,9	314,86
	20	Day 1	180	180,9	180,9	531,1	531,1	532,1	532,1	532,1	533,1	314,86	314,9	314,86
	25	Day 1	180	180,9	180,9	531,1	531,1	531,1	533,1	532,1	532,1	314,86	313,9	314,86

Range	353,2
Cp-gauge	134,6

Gauge Capability Cp	Conclusion Gauge evaluation
<5	Unacceptable
5-10	Marginal / Poor
10-50	Acceptable
50-100	Good
>100	Excellent

Design of experiments KOH

ANOVA-Table

Factor /	SS	DoF	MS	F - value	F -Critical	P-value	Conclusion
A	7	1	6,93	48	4,41	0,017	significant
B	740262	1	740262	5077688	4,41	5,51E-43	significant
AB	2	1	2,01	14	4,41	0,173	significant
C	5	1	4,96	34	4,41	0,039	significant
AC	2	1	2,01	14	4,41	0,173	significant
BC	2	1	2,01	14	4,41	0,173	significant
ABC	0	1	0,37	3	4,41	0,551	
Curve	4529	1	4528,6	31063	4,41	4,44E-23	significant
Error	3	18	0,15	X	X	X	X
Total	744812	26	28647	X	X	X	X

Factor name
A: Temperature
B: Current
C: Flow rate

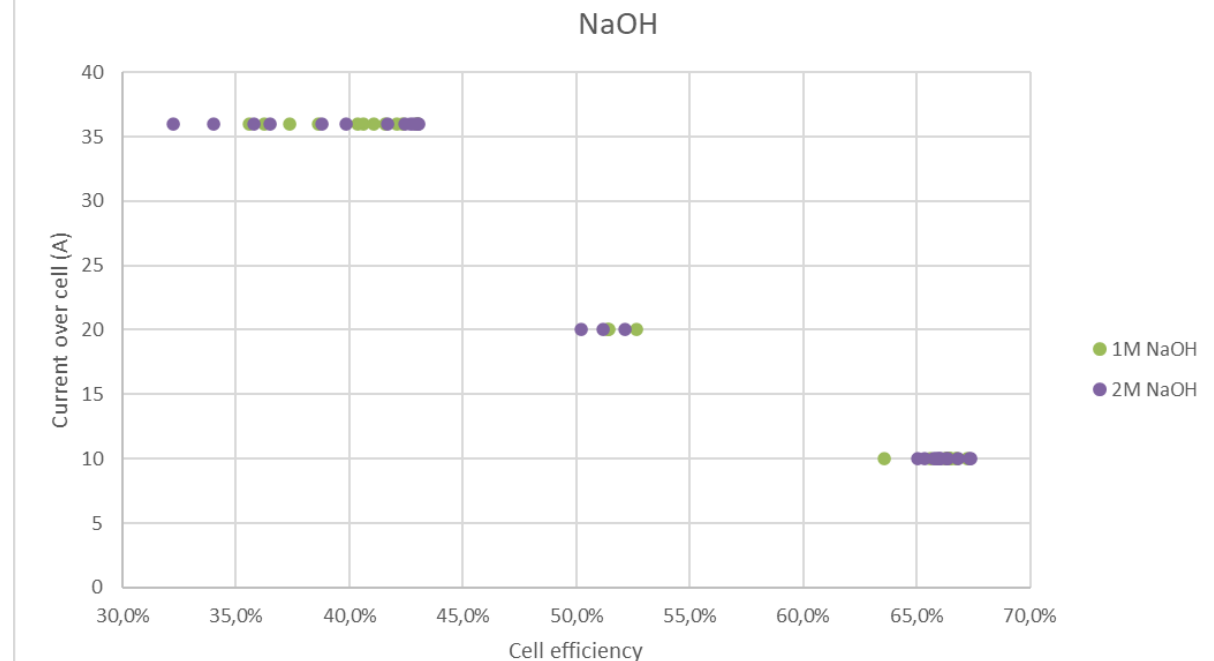
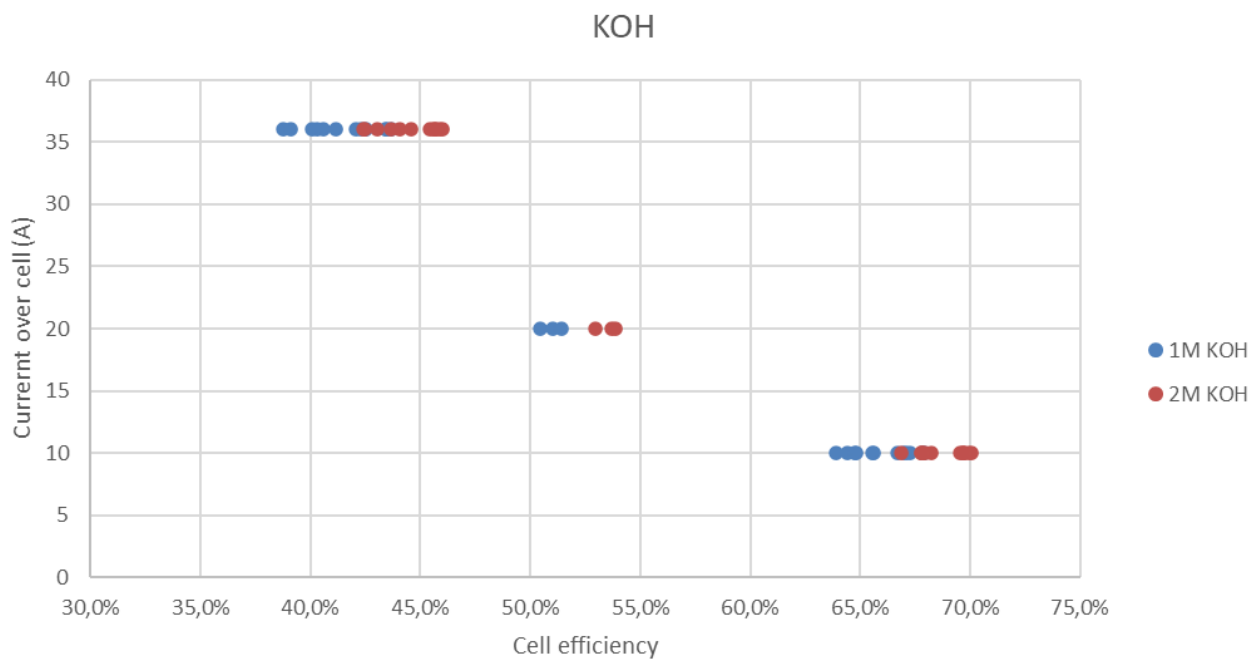
Design of experiments NaOH

ANOVA-Table

Factor /	SS	DoF	MS	F - value	F -Critical	P-value	Conclusion	
A	0	1	0,04	1	4,41	0,842		
B	743751	1	743751	10203233	4,41	5,282E-43	significant	
AB	0	1	0,04	1	4,41	0,842		
C	0	1	0,04	1	4,41	0,842		
AC	0	1	0,04	1	4,41	0,842		
BC	0	1	0,04	1	4,41	0,842		
ABC	0	1	0,04	1	4,41	0,842		
Curve	4384	1	4384,4	60148	4,41	5,934E-23	significant	
Error	1	18	0,07	X	X	X	X	X
Total	748137	26	28774	X	X	X	X	X

Factor name
A: Temperature
B: Current
C: Flow rate

Design of experiments cell efficiency



Conclusions

- The kaliumhydroxide is better lye for the production of hydrogen
 - Higher efficiency
 - Less heat build up
- Influence of hydrogen production
 - Current (High influence)
 - Temperature
 - Flow rate
- Better efficiency
 - KOH lye solution (higher molair the better)
 - Less current on the elektrolyser cell

Project HYGENESYS – Simulatie model alkaline elektrolyser en verificatie

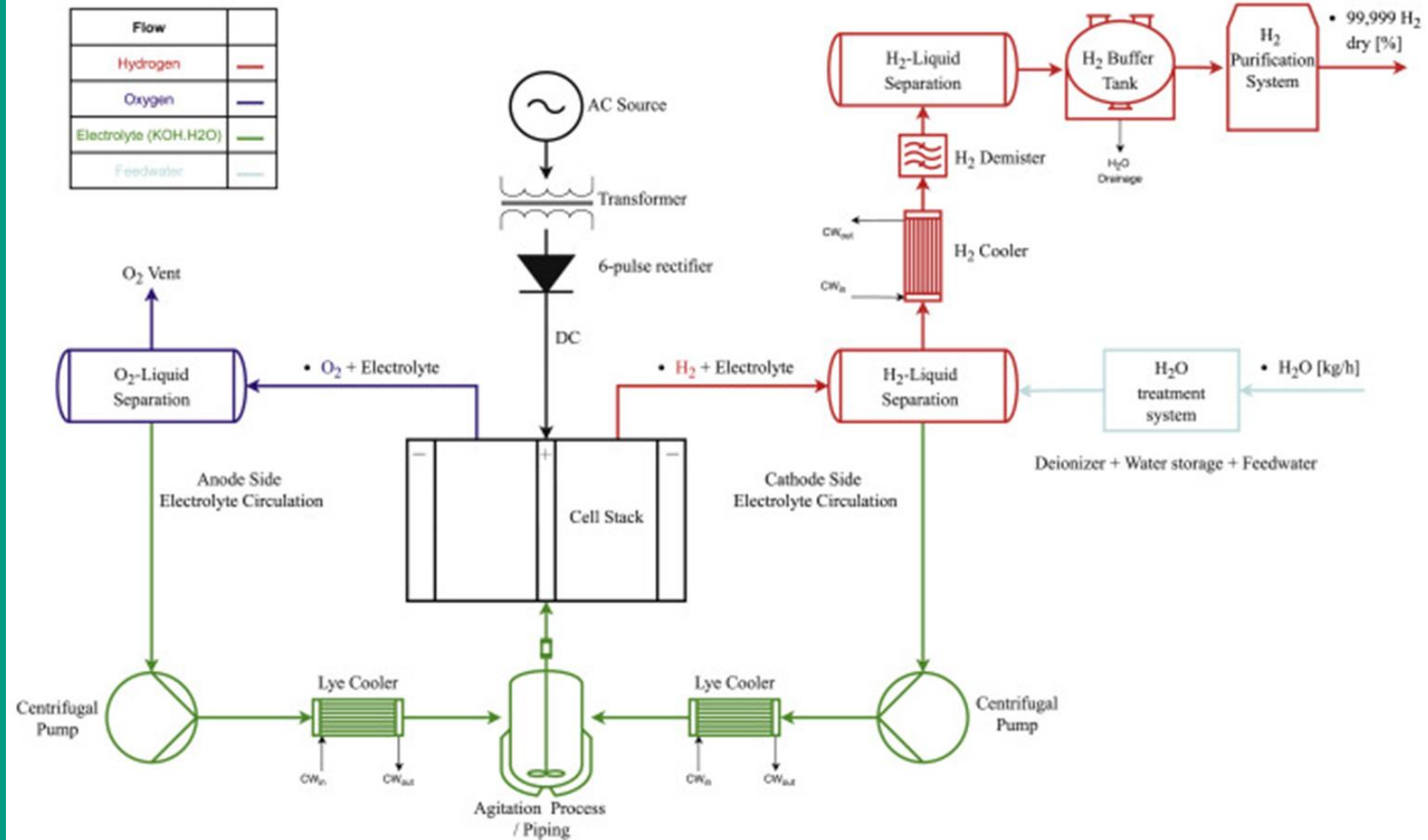
Bas Hupjé

4^{de} jaars student Chemische Technologie



The system

- Assumptions:
 - Steady state
 - Current determines hydrogen production
 - The incoming electrolyte flow cools the stack
 - The splitters are modeled with a split factor
 - Gas does not dissolve in liquid
 - Mixed phase elektrolyser



Matlab

- Programming in Matlab

The screenshot displays the MATLAB R2022b environment. The main window shows a script named 'Elektrolyser_script.m' with the following code:

```
68 Cp_KOH = Cp_KOH_mol/MolarmassKOH; %Heat capacity KOH (kJ/(kg*K))
69 Cp_H2O = 4.1969; %Heat capacity water (kJ/(kg*K))
70 Cp_elec = 4.07; %Heat capacity in flow elektrolyser (KJ/(kg*K))
71
72 %Production rate stack in moles per second
73 N_hydrogen = Ecell*Nf*icell*Aeff/(z*F); %Hydrogen production at the stack (mol/s)
74 N_H2O_prod = N_hydrogen; %Water production at the stack (mol/s)
75 N_OH = 2 * N_hydrogen; %OH production at the stack (mol/s)
76 N_O2 = 0.5 * N_hydrogen; %Oxygen production at the stack (mol/s)
77 N_H2O_cons = 2 * N_hydrogen; %Water consume at the stack (mol/s)
78 N_OH_cons = N_OH; %OH consume at the stack (mol/s)
79
80 %Production rate in kilograms per second
81 Prod_H2 = N_hydrogen * MolarmassH2 * 10^-3; %Hydrogen production at the stack (kg/s)
82 Prod_H2O = N_H2O_prod * MolarmassH2O * 10^-3; %Water production at the stack (kg/s)
83 Prod_OH = N_OH * MolarmassOH * 10^-3; %OH production at the stack (kg/s)
84 Prod_O2 = N_O2 * MolarmassO2 * 10^-3; %Oxygen production at the stack (kg/s)
85 Cons_H2O = N_H2O_cons * MolarmassH2O * 10^-3; %Water consume at the stack (kg/s)
86 Cons_OH = N_OH_cons * MolarmassOH * 10^-3; %OH consume at the stack (kg/s)
87
88 %Molarity determining
89 Mass_KOH_per_liter = Perc_KOH_stack/(Perc_H2O_stack * RhoH2O * 10^-3); %The mass KOH in 1 liter of H2O
90 MKOH = Mass_KOH_per_liter/(MolarmassKOH * 10^-3); %moles KOH in 1 liter H2O (mol/l)
91
92
```

The Command Window shows the following output:

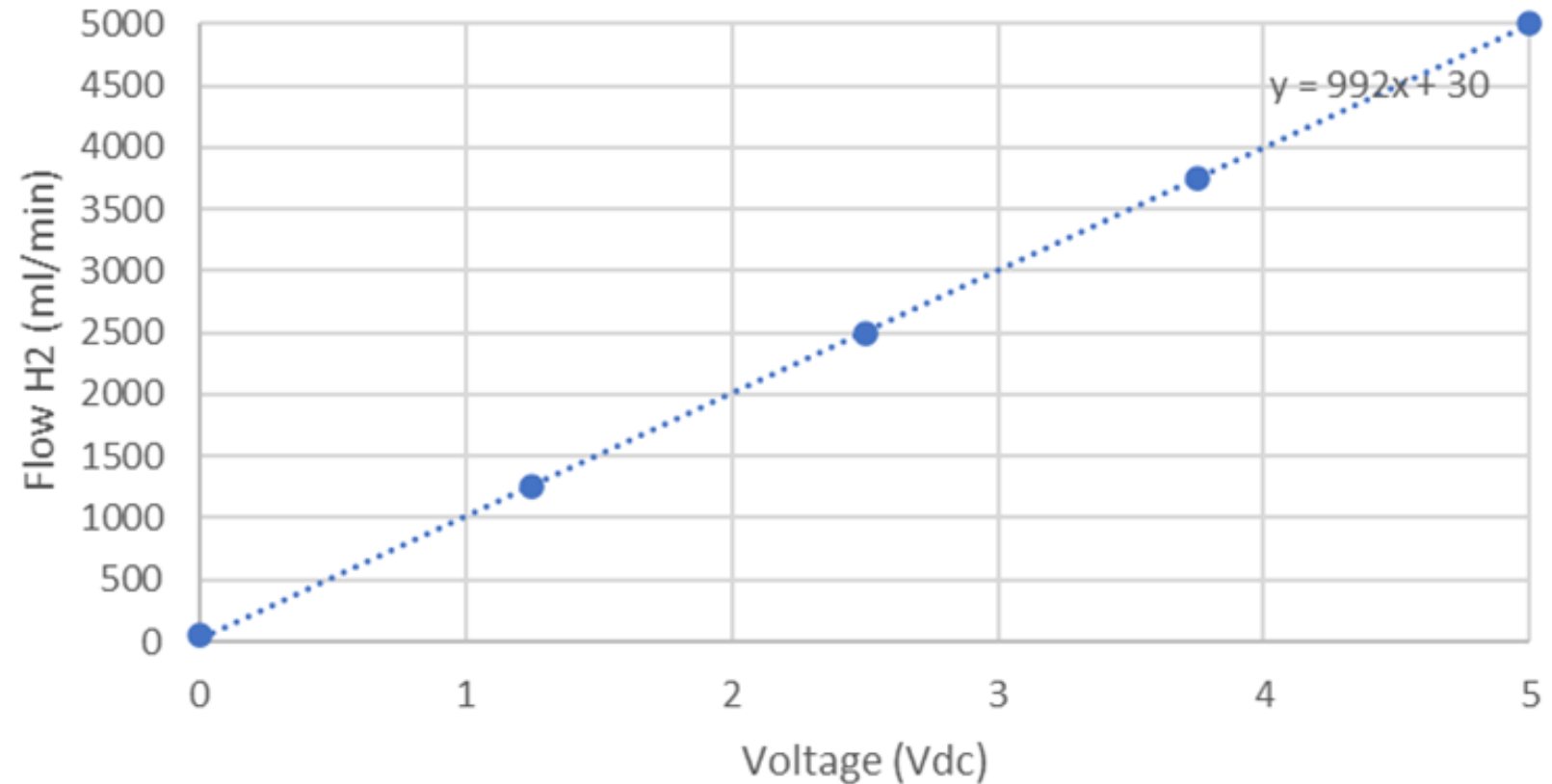
Felec_in_H2O	H2O_cat_out	H2O_an_out	H2O_storage_cat	H2O_split_cat_out	H2O_split_in	H2O_storage_an	H2O_split_ar
23.118	11.081	11.798	0	11.32	0.2391	0	11.798

The Workspace window on the right lists various variables and their values, including 'a' (-0.1446), 'a1' (0.8000), 'a2' (-0.0076), 'Aeff' (2.6600), 'aH2OKOH' (0.6834), 'ans' (1x9 table), 'Astack' (33.8161), 'b' (1.0110), 'b1' (20), 'b2' (0.1000), 'b3' (350000), 'Cbolz' (5.6704e-08), 'Cons_H2O' (0.4782), 'Cons_OH' (0.4515), 'Cp_elec' (4.0700), 'Cp_H2O' (4.1969), 'Cp_HE_an' (3.5204), 'Cp_HE_cat' (3.3641), 'Cp_KOH' (1.1740), 'Cp_KOH_mol' (65.8700), 'D' (1.8400), 'Ecell' (326), 'emiss' (0.8000), 'F' (96485), 'F_HE_an_c' (4.2499), 'F_HE_an_h' (15.1996), 'F_HE_cat_c' (4.1747), 'F_HE_cat_h' (15.6244), 'Felec_in' (30.8240), 'Felec_in_H2O' (23.1180), 'Felec_in_KOH' (7.7060), 'h' (3.0153), and 'H2_an_in' (0).

Calibration flowmeter

- At a flow of 50 ml/min no voltage is measured
- The working area of the sensor is not the same as the working area of the setup
- 2 Methods used to determine the size of hydrogen production:
 - 1: Flow = 1000*voltage
 - 2: Flow = 960*voltage + 50

Calibratiegrafiek bronkhorst h2 sensor 3S

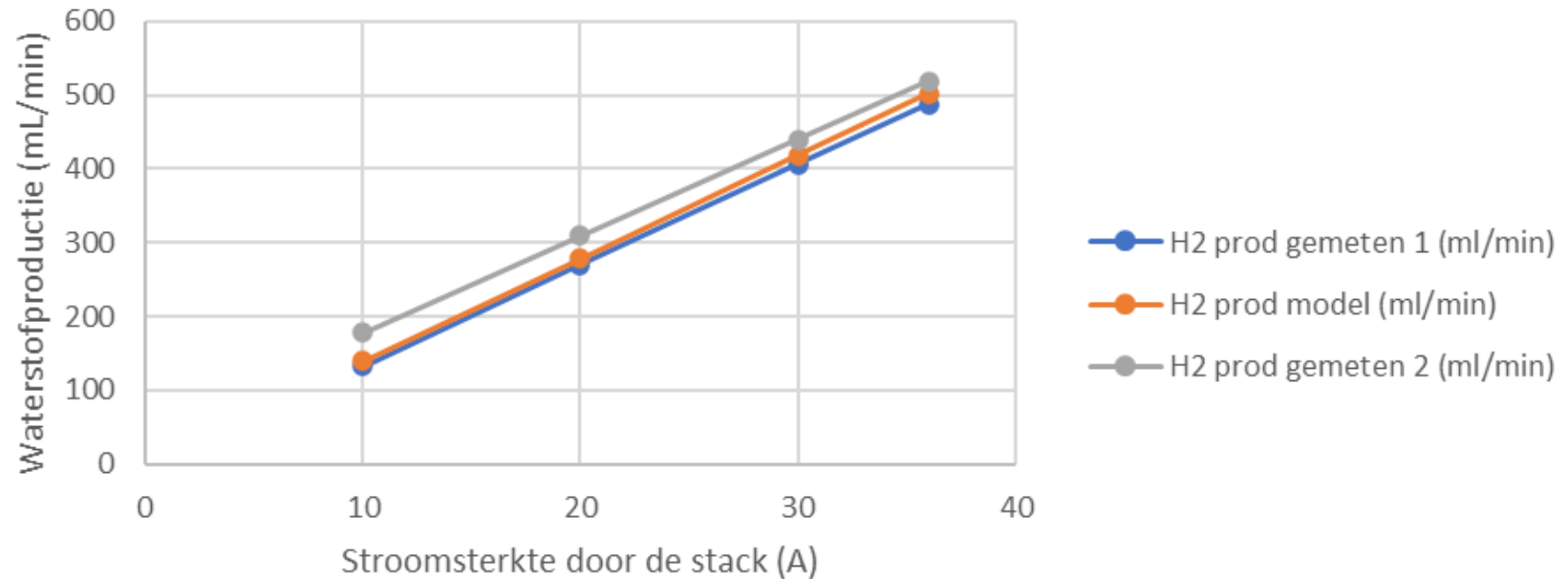


H₂ production vs the current

- H₂ prod measured 1
 - Flow = 1000*voltage
- H₂ prod measured 2
 - Flow = 960*voltage + 50
- H₂ prod model in between the 2 lines of H₂ production

$$nH_2 = Ec \left(nf * \frac{i_{cell} * A_{eff}}{z * F} \right)$$

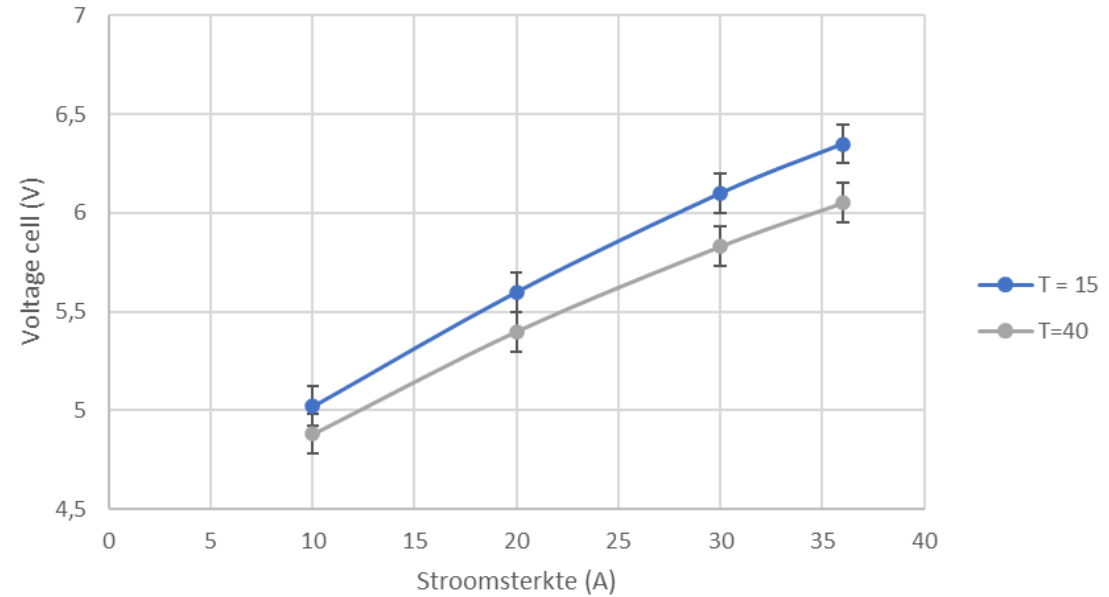
Waterstof productie ten opzichte van de stroomsterkte
T = 40C F = 7,33 l/min



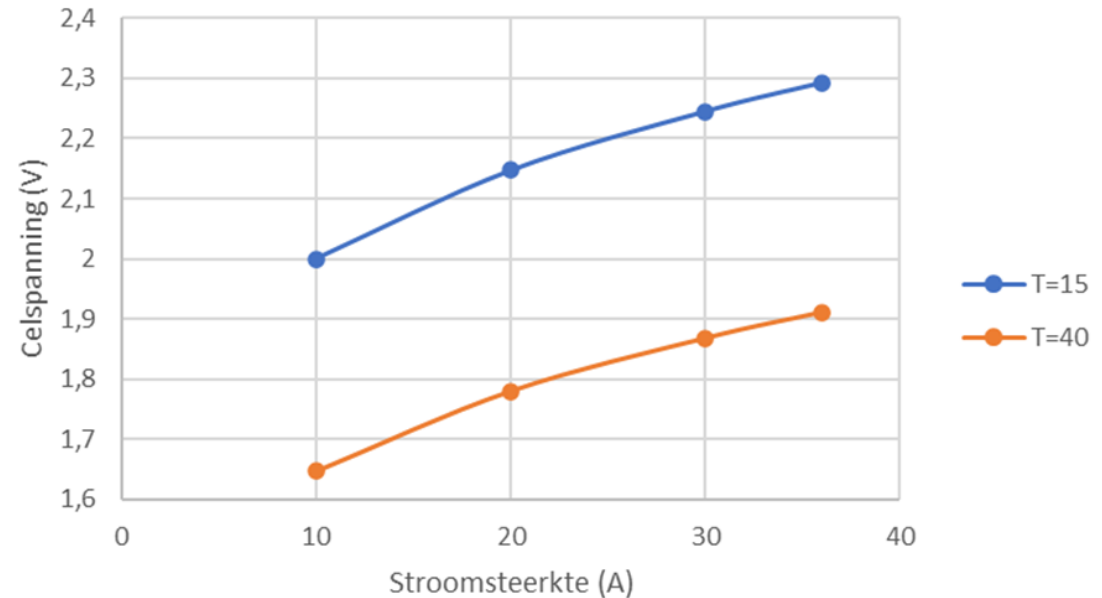
H₂ production vs temperature

- Temperature and H₂ production linked by Nernst equation
- Reversible voltage linked to the cell voltage
- Cell voltage linked to efficiency with thermo-neutral voltage
- Efficiency = U_{tn}/U_{cell}
- The curves of the model and the measurements give the same course

IV curve bij een flow van 7,33 L/min en F = 1



IV curve model



Conclusions

- Model matches literature quite well
- Model matches well with the measurements
- The higher the current, the more H₂ produced
- Higher temperature leads to higher efficiency

Questions?

